Week 13

Lecture 1

 Mechanical Energy Reservoir (MER) is a reservoir for organized mechanical energy. MER is open to work transfer only. Its walls are adiabatic $dQ = 0$. It is entropy free.

$$
dS = 0 \quad \text{for a} \quad \text{MER}
$$

 Entropy Change for a Control Mass (CM). Isolated system. CM interacts with TER and MER, and $P_S \geq 0$

$$
dS_{CM}+dS_{TER}+dS_{MER}=d\mathcal{P}_{S}\geq 0
$$

but $dS_{MER} = 0$ and $dS_{TER} = -dQ/T_{TER}$. Therefore

$$
dS_{CM}-\frac{dQ}{T_{TER}}=d\mathcal{P}_{S}\geq 0
$$

 \mathcal{P}_S is not a property. It depends on the process path just like Q and W.

SLOT for CM

$$
dS_{CM}=\frac{dQ}{T_{TER}}+d\mathcal{P}_{S}
$$

where the terms represent:

- Increase in entropy storage within CM
- Entropy inflow in CM
- Entropy production
- Integrating gives the total entropy change in CM

$$
(S_2 - S_1)_{\text{CM}} = \frac{Q_{1\rightarrow 2}}{T_{TER}} + (\mathcal{P}_S)_{1\rightarrow 2}
$$

But

$$
\left({\mathcal{P}}_S\right)_{1\to2}\geq 0
$$

where > 0 is the real world, and $= 0$ when all processes within isolated system are reversible (frictionless, loss less, etc).

 \bullet (β)_{1→2} = 0 will be used to determine:

- Maximum efficiency of a cyclic device
- Minimum work reqired to run a pump
- Maximum work that can be obtained from a given system
- For any Control Mass, Reversible, Adiabatic Process

$$
dS_{CM}=0\quad \Delta S_{CM}=S_2-S_1=0
$$

Lecture 2

- Last lecture of the term.
- Last tutorial today.
- Final examination scheduled for Friday, August 6 from 9:00 to 12:00 Noon.

 Open book exam: text, lecture notes, notes from the ECE 309 Web site, and calculator. Five questions of equal value. There will be at least one heat transfer question.

SLOT/CV

$$
\dot{\mathcal{P}}_S = \frac{\partial}{\partial t} S_{CV} - \dot{S}_{in} + \dot{S}_{out} + \sum_{i=1} \left(\frac{\dot{Q}_i}{T_i}\right)_{CV}
$$

where

$$
\frac{\partial}{\partial t}S_{CV} = \frac{\partial}{\partial t}\int_{CV}s\rho dV
$$

and

$$
\dot{S}_{in} = \int_{A_{in}} s \rho \vec{V} \cdot \vec{n} \ dA \quad \textrm{and} \quad \dot{S}_{out} = \int_{A_{out}} s \rho \vec{V} \cdot \vec{n} \ dA
$$

Alternative Form of SLOT/CV

$$
\left(\frac{dS}{dt}\right)_{CV} = \left(s\dot{M} + \frac{\dot{Q}}{T}\right)_{in} - \left(s\dot{M} + \frac{\dot{Q}}{T}\right)_{out} + \dot{\mathcal{P}}_S
$$

- Example of a SSSF System
- Boiler and Turbine. Find W_{max}
- Continuity Equation (Conservation of Mass)

 \sim \sim \sim \sim

$$
\dot{M}_{in}=\dot{M}_{out}=\dot{M}
$$

• Define Control Volume with inflows and outflows.

 \mathbf{r}

 \bullet FLOT/CV

$$
\left(\frac{dE}{dt}\right)_{CV}=\dot{Q}-\dot{W}+\left(\dot{M}h\right)_{in}-\left(\dot{M}h\right)_{out}
$$

and

$$
\left(\frac{dE}{dt}\right)_{CV}=0
$$

SLOT/CV

$$
\left(\frac{dS}{dt}\right)_{CV} = \left(\dot{M}s + \frac{\dot{Q}}{T_R}\right)_{in} - \left(\dot{M}s\right)_{out} + \dot{\mathcal{P}}s
$$

$$
\left(\frac{dS}{dt}\right)_{in} = 0
$$

and

$$
\left(\frac{dS}{dt}\right)_{CV} =
$$

onving for α we find

$$
\dot{Q} = \left[\left(\dot{M}s\right)_{out}-\left(\dot{M}s\right)_{in}-\dot{\mathcal{P}}_S\right]T_R
$$

Substitute into FLOT equation and solve for \dot{W}

$$
\dot{W}=\left\{\dot{M}\left(h-T_{R}s\right)_{in}-\dot{M}\left(h-T_{R}s\right)_{out}\right\}-T_{R}\dot{\mathcal{P}}_{S}
$$

 \bullet Definition of Specific Availability b

$$
b=h-T_R s
$$

Now

$$
\dot{W}=\dot{M}(b_{in}-b_{out})-T_R\dot{\mathcal{P}}_S \quad \text{and} \quad \dot{\mathcal{P}}_S\geq 0
$$

Therefore

$$
\dot{W} \leq \dot{M}(b_{in}-b_{out})
$$

 \bullet Maximum I ower W_{max} occurs when $PS = 0$

$$
\dot{W}_{max} = \dot{M}(b_{in} - b_{out})
$$

• $b = h - T_R s$ is also called the Exergy.

A 2T Heat Engine

- undergoes a cycle
- receives Q_A from heat source at temperature T_A
- rejects heat Q_B to a heat sink at temperature T_B
- $-$ output is work W
- \bullet Energy Conversion Efficiency η

$$
\eta = \frac{W(\text{work out})}{Q_A(\text{input})} < 1
$$

$$
\eta = \frac{\dot{W}({\rm power~out})}{\dot{Q}_{A}({\rm input~rate})} < 1
$$

- \bullet Carnot Efficiency
- $-$ Steady-state
- Zero inflow and outflow: $M_{in} = M_{out} = 0$
- T_{A} and T_{B} are constant
- \bullet Apply FLOT/CV and SLOT/CV

 λ

FLOT/CV

$$
\left(\frac{dE}{dt}\right)_{CV} = \dot{Q}_A - \dot{Q}_B - \dot{W} + \left(\dot{M}h\right)_{in} - \left(\dot{M}h\right)_{out}
$$

However

$$
\left(\frac{dE}{dt}\right)_{CV} = 0, \quad \left(\dot{M}h\right)_{in} = 0, \quad \left(\dot{M}h\right)_{out} = 0
$$

and

$$
\dot{W} = \dot{Q}_A - \dot{Q}_B
$$

• SLOT/CV

$$
\left(\frac{dS}{dt}\right)_{CV} = \left(\dot{M}s + \frac{\dot{Q}_A}{T_A}\right)_{in} - \left(\dot{M}s + \frac{\dot{Q}_B}{T_B}\right)_{out} + \dot{\mathcal{P}}_S
$$

However

$$
\left(\frac{dS}{dt}\right)_{CV} = 0, \quad \left(\dot{M}s\right)_{in} = 0, \quad \left(\dot{M}s\right)_{out} = 0
$$

Therefore

$$
\frac{\dot{Q}_A}{T_A}-\frac{\dot{Q}_B}{T_B}+\dot{\mathcal{P}}_S=0
$$

and $\textit{rs}\geq 0.$

- Assume neversible Heat Engine: $\forall s = 0$
- \bullet Heat Rejection to Heat Sink

$$
\dot{Q}_B = \dot{Q}_A \frac{T_B}{T_A}
$$

 \bullet Carnot Efficiency

$$
\eta = \frac{\dot{W}}{\dot{Q}_A} = \frac{\dot{Q}_A - \dot{Q}_B}{\dot{Q}_A} = 1 - \frac{\dot{Q}_B}{\dot{Q}_A} = 1 - \frac{T_B}{T_A} < 1
$$

 \bullet Carnot efficiency is upper limit on efficiency of real heat engines.

• Example: If heat is rejected to environment at $I_b = 285$ K, and if the heat source is combustion gases at $T_A = 2000 \text{ K}$, calculate the Carnot emclency.

$$
\eta=1-\frac{285}{2000}=0.858
$$

• Metalurical limits the source temperature to $T_A = 1000 K$, now calculate the Carnot efficiency.

$$
\eta=1-\frac{285}{1000}=0.715
$$

Most modern power plants operate at efficiencies between $40 - 50\%$.