

## Week 4

### Lecture 1

Hand out Project 1. Due Friday, October 16, 12 Noon.

- Extended surfaces or fins; temperature is one-dimensional  $T(x)$  when  $Bi = ht_e/k < 0.2$  where the effective fin thickness is defined as  $t_e = A/P$ ; where  $P$  is the constant fin perimeter and  $A$  is the constant fin conduction area.

See Web Site for derivation of general fin equation and general solution for fins with contact conductance,  $h_c$ , and end cooling,  $h_e$ ;

solution  $\theta(x) = T(x) - T_f$ , called the temperature excess, is a function of dimensionless parameters:  $Bi_c = h_c L/k$ ,  $Bi_e = h_e L/k$ ,  $mL$  with fin parameter:  $m = \sqrt{hP/(kA)}$

$P$  is the constant fin perimeter and  $A$  is the constant fin conduction area.

- Fin resistance:  $R_{\text{fin}} = \theta_b/Q$ ;  $\theta_b = T_b - T_f$ .

- Special cases of the general solution:

(a) perfect contact at fin base:  $Bi_c = \infty$  and end cooling:  $Bi_e > 0$

(b) perfect contact at fin base:  $Bi_c = \infty$  and adiabatic end:  $Bi_e = 0$ ;

(c) perfect contact and *infinitely long* fin.

- Criterion for *infinitely long* fin:  $L_{\text{crit}} = 2.65/\sqrt{(hP/kA)}$

When  $L > L_{\text{crit}}$ , model fin as *infinitely long*, and when  $L < L_{\text{crit}}$ , model fin as finite length with end cooling.

### Lecture 2

- Show examples of pin fins, straight fins and circular annular fins from telecommunication and microelectronics industries, and automotive industries.

- Sketch the typical straight fin (straight or pin) of length,  $L$ , conduction area,  $A$ , and perimeter,  $P$ .

- End conditions: (i) contact conductance,  $h_c$  at the base,  $x = 0$ , and (ii) convective cooling at the end,  $x = L$ .

- When  $Bi = ht_e/k < 0.2$ , then  $T(x, y) \rightarrow T(x)$ .

- Derivation of ODE:

★ heat balance on differential control volume (CV)  $dV = Adx$ :

★ conduction into CV at  $x$  is  $dQ_x = -kAdT/dx$ ,

- \* conduction rate out of CV at  $x + dx$  is  $Q_x + (dQ_x/dx) dx$ ,
  - \* convection loss is  $dQ_{\text{conv}} = hP dx(T(x) - T_f)$ ;
  - \* no sources, steady-state;
  - \* derive governing second-order ordinary differential equation.
- see section 3.6.2 for derivation of ODE and boundary conditions at  $x = 0$  (perfect contact) and  $x = L$  (convection cooling).
- See Table 3.4 for summary of solutions.
  - See Table 3.5 for summary of fin efficiencies:  $\eta_f$  for various fin types.

### Lecture 3

Review of material on Web site for derivation of general fin equation valid for variable conduction area,  $A(x)$ , and variable perimeter,  $P(x)$ ; introduce temperature excess:  $\theta(x) = T(x) - T_f$ ; note that  $d\theta/dx = dT/dx$  because  $T_f$  is constant; consider special case:  $A$  and  $P$  are constants;

fin equation becomes  $d^2\theta/dx^2 - m^2\theta = 0$  in  $0 < x < L$  with fin parameter:

$$m = \sqrt{hP/kA} \quad \text{units of } m \text{ are } 1/m;$$

at the base,  $x = 0$ , there is contact conductance,  $h_c$ , and at the fin end,  $x = L$ , there is convective cooling,  $h_e$ ;

boundary conditions of the third kind (Robin) are applied at the fin base and fin end:

$$d\theta(0)/dx = -(h_c/k)[\theta_b - \theta(0)] \quad \text{and} \quad d\theta(L)/dx = -(h_e/k)\theta(L); \quad \theta_b = T_b - T_f;$$

solution is  $\theta = C_1 \cosh mx + C_2 \sinh mx$ ;

introduce dimensionless fin parameters:  $Bi_c = h_c L/k$ ,  $Bi_e = h_e L/k$ ,

$$mL = \sqrt{(hP/kA)} L$$

solve for the constants of integration which are:

$$C_1 = \frac{\theta_b}{1 + \frac{mL\phi}{Bi_c}} \quad \text{and} \quad C_2 = -\frac{\theta_b\phi}{1 + \frac{mL\phi}{Bi_c}}$$

where

$$\phi = \frac{mL \tanh mL + Bi_e}{mL + Bi_e \tanh mL}$$

obtain fin heat flow rate:  $Q_{\text{fin}} = -kA_b d\theta(0)/dx$ ;  $A_b$  is the base conduction area.

fin resistance:  $R_{\text{fin}} = \theta_b/Q_{\text{fin}}$ ; see Web Site for development of solution and use the Javascript Calculator;

perfect contact at base and end cooling:

$$R_{fin} = 1/\sqrt{hPkA} \tanh mL$$

perfect contact at fin base and *infinitely long fin*:

$$R_{fin} = 1/\sqrt{hPkA}$$

fin efficiency:  $\eta_f = Q_{fin}/Q_{ideal}$ ;

$Q_{ideal}$  corresponds to an ideal fin whose thermal conductivity is infinitely large

$$Q_{ideal} = \int_0^L hP\theta_b dx + h_e A\theta_b = (hPL + h_e A)\theta_b$$

special cases of general solution with perfect contact at fin base:

$$h_c = \infty \text{ or } Bi_c = \infty;$$

three options at the fin end:

(i) end cooling  $h_e > 0$  or  $Bi_e > 0$ ;

(ii) adiabatic end:  $h_e = 0$  or  $Bi_e = 0$ ;

(iii) *infinitely long fin*, i.e.  $L > L_{crit} = 2.65/\sqrt{hP/kA}$ ;

see Web Site for several special cases.

Longitudinal fins; pin fins; circular annular fins; analytical solutions for several types of fins; see Table 3.5 for efficiencies of common fin shapes.

Applications of fin solutions:

- example 1 is a circular rod of length  $2L$  which connects two walls at temperatures  $T_1$  and  $T_2$  which are greater than air temperature  $T_f$ ; there is convective cooling from the sides of the rod into the air. Assume perfect contact at the interfaces between the rod and the two walls.

special cases:

(i) when  $T_1 = T_2$ , the plane of symmetry (adiabatic plane) occurs at mid-point

(ii) when  $T_1 > T_2$ , the plane of symmetry moves to the right of the mid-point

(iii) when  $T_1 < T_2$ , the plane of symmetry moves to the left of the mid-point

- example 2 is a system which consists of two finite length fins  $L_1, L_2$  with adiabatic ends connected to a rod of length  $L_3$  with adiabatic lateral boundaries. Check Biot numbers: is  $Bi_1 = h_1 t_e/k < 0.2$  and is  $Bi_2 = h_2 t_e/k < 0.2$ ? Yes.

- system heat transfer rate:  $Q_{sys} = (T_{f1} - T_{f2})/R_{sys}$

- system resistance:  $R_{sys} = R_{fin1} + R_{rod} + R_{fin2}$

- component resistances:

$$R_{fin1} = 1/\sqrt{h_1 P k A} \tanh(m_1 L_1) \text{ and } m_1 = \sqrt{h_1 P/(kA)}$$

$$R_{fin2} = 1/\sqrt{h_2 P k A} \tanh(m_2 L_2) \text{ and } m_2 = \sqrt{h_2 P/(kA)}$$

$$R_{rod} = L_3/(kA)$$


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