## ECE 309

## Introduction to Thermodynamics and Heat Transfer

## Tutorial \# 6

## Entropy

## Problem 1

Air is compressed steadily by a $5-\mathrm{kW}$ compressor from 100 kPa and $17^{\circ} \mathrm{C}$ to 600 kPa and $167^{\circ} \mathrm{C}$ at a rate of $1.6 \mathrm{~kg} / \mathrm{min}$. During this process, some heat transfer takes place between the compressor and the surrounding medium at $17^{\circ} \mathrm{C}$. Determine
(a) the rate of entropy change of air and
(b) the rate of entropy generation during this process.


## Solution:

Step 1: Write the given data from the problem statement
State 1: $P_{1}=100 \mathrm{kPa}, \quad T_{1}=17^{\circ} \mathrm{C}$
State 2: $P_{2}=600 \mathrm{kPa}, T_{2}=167^{\circ} \mathrm{C}$
Surrounding temperature: $T_{\text {surr }}=17^{\circ} \mathrm{C}$
Work input to the compressor: $\dot{W}=-5 \mathrm{~kW}$ (negative sign indicates work is done on the system)
Mass flow rate: $\dot{m}_{1}=\dot{m}_{2}=\dot{m}=1.6 \mathrm{~kg} / \mathrm{min}=0.02666 \mathrm{~kg} / \mathrm{s}$
Step 2: Write what we are asked to solve for:
(a) rate of entropy change of air: $\Delta \dot{S}_{\text {air }}=$ ?
(b) rate of entropy generation during the process: $\dot{S}_{g e n}=$ ?

## Step 3: State the assumption(s):

(1) At the specified conditions air can be assumed as an ideal gas
(2) Assuming steady state steady flow process (SSSF)
(3) Changes in kinetic and potential energies to be negligible

Step 4: Write the Energy balance (First Law of Thermodynamics) and Entropy Balance (Second Law of Thermodynamics) equations for the system shown in Figure P1

Energy Balance (First Law of Thermodynamics):
$\dot{Q}-\dot{W}=\dot{m}\left(h_{2}-h_{1}\right)$
for ideal gas, we know that
$d h=C_{p, a v} d T$
$\dot{Q}=\dot{W}+\dot{m} C_{p, a v}\left(T_{2}-T_{1}\right)$

Entropy Balance (Second Law of Thermodynamics):
$\sum \frac{\dot{Q}}{T}+\dot{S}_{g e n}=\dot{m}\left(s_{2}-s_{1}\right)$
Again for ideal gas, we know that
$s_{2}-s_{1}=C_{p, a v} \ln \frac{T_{2}}{T_{1}}-R \ln \frac{P_{2}}{P_{1}}$
where R is gas constant

$$
\begin{equation*}
\sum \frac{\dot{Q}}{T}+\dot{S}_{g e n}=\dot{m}\left(C_{p, a v} \ln \frac{T_{2}}{T_{1}}-R \ln \frac{P_{2}}{P_{1}}\right) \tag{1.6}
\end{equation*}
$$

Step 5: Solve for the unknown quantities
From Eq. (1.3), calculate the heat transfer during the process
$\dot{Q}=-5 \mathrm{~kW}+(0.02666 \mathrm{~kg} / \mathrm{s})(1.010 \mathrm{~kJ} /(\mathrm{kg} \cdot \mathrm{K}))(440-290) K=-0.96101 \mathrm{~kW}$
Note: In the above calculation of heat transfer, $\mathrm{C}_{\mathrm{p}, \mathrm{av}}$ is found from Table A-2b at $\mathrm{T}_{\mathrm{av}}=365 \mathrm{~K}$
(a) Rate of entropy change $\left(\Delta \dot{S}_{\text {air }}\right)$
$\Delta \dot{S}_{a i r}=\dot{m}\left(s_{2}-s_{1}\right)=\dot{m}\left(C_{p, a v} \ln \frac{T_{2}}{T_{1}}-R \ln \frac{P_{2}}{P_{1}}\right)$
where $s_{2}-s_{1}$ is replaced by Eq. (1.5)

$$
\Delta \dot{S}_{\text {air }}=(0.02666 \mathrm{~kg} / \mathrm{s})\left((1.010 \mathrm{~kJ} / \mathrm{kg} \cdot \mathrm{~K}) \ln \frac{440 \mathrm{~K}}{290 \mathrm{~K}}-(0.287 \mathrm{~kJ} / \mathrm{kg} \cdot \mathrm{~K}) \ln \frac{600 \mathrm{kPa}}{100 \mathrm{kPa}}\right)(1.9)
$$

$$
\Delta \dot{S}_{\text {air }}=-0.00248 \mathrm{~kW} / \mathrm{K}
$$

(b) Rate of entropy generation during the process ( $\dot{S}_{\text {gen }}$ )

Using Eq. (1.6) and result (a), we can find the rate of entropy generation during the process

$$
\begin{equation*}
\dot{S}_{\text {gen }}=\Delta \dot{S}_{\text {air }}-\frac{\dot{Q}}{T_{\text {surr }}}=-0.00248 \mathrm{~kW} / \mathrm{K}-\frac{-0.96101 \mathrm{~kW}}{290 \mathrm{~K}} \tag{1.10}
\end{equation*}
$$

$\dot{S}_{\text {gen }}=0.00083 \mathrm{~kW} / \mathrm{K}$

## Problem 2

Steam enters a turbine at 30 bars and $400^{\circ} \mathrm{C}$ with a velocity of $160 \mathrm{~m} / \mathrm{s}$. Saturated vapor exits at $100^{\circ} \mathrm{C}$ with a velocity of $100 \mathrm{~m} / \mathrm{s}$. At steady state, the turbine develops work equal to 540 kJ per kg of steam flowing through the turbine. Heat transfer between the turbine and its surroundings occurs at an average outer surface temperature of 500 K Determine the rate at which entropy is produced within the turbine per kilogram of steam flowing, in $\mathrm{KJ} / \mathrm{kgK}$. Neglect the change in potential energy between inlet and exit.

## Solution:

Step 1: Write the given data from the problem statement
State 1: $P_{1}=30$ bars, $T_{1}=400^{\circ} \mathrm{C}, \mathrm{V}_{1}=160 \mathrm{~m} / \mathrm{s}$
State 2: Saturated vapor, $T_{2}=100^{\circ} \mathrm{C}, \mathrm{V}_{2}=100 \mathrm{~m} / \mathrm{s}$


Figure P2
Boundary temperature: $T_{b}=500 \mathrm{~K}$
W ork output from the turbine: $W=540 \mathrm{~kJ} / \mathrm{kg}$

## Step 2: Write what we are asked to solve for:

Rate of entropy produced per kg of steam flowing within the turbine: $S_{\text {gen }}=$ ?

## Step 3: State the assumption(s):

(1) Assuming steady state steady flow process (SSSF)
(2) Change in potential energy between the inlet and outlet is negligible
(3) Heat transfer between the turbine and the surroundings occurs at a boundary temperature $\mathrm{T}_{\mathrm{b}}$

Step 4: Write the Energy balance (First Law of Thermodynamics) and Entropy Balance (Second Law of Thermodynamics) equations for the system shown in Figure P2

Energy Balance (First Law of Thermodynamics):
$\dot{Q}-\dot{W}=\dot{m}\left(h_{2}-h_{1}+\frac{V_{2}^{2}-V_{1}^{2}}{2}\right)$
$\frac{\dot{Q}}{\dot{m}}=\frac{\dot{W}}{\dot{m}}+h_{2}-h_{1}+\frac{V_{2}^{2}-V_{1}^{2}}{2}$
$Q=\frac{\dot{Q}}{\dot{m}}=W+h_{2}-h_{1}+\frac{V_{2}^{2}-V_{1}^{2}}{2}$
$Q=540\left(\frac{k J}{k g}\right)+(2676.1-3230.9)\left(\frac{\mathrm{kJ}}{\mathrm{kg}}\right)+\left(\frac{100^{2}-160^{2}}{2}\right)\left(\frac{\mathrm{m}^{2}}{\mathrm{~s}^{2}}\right)\left(\frac{1 \mathrm{~N}}{1 \frac{\mathrm{~kg} m}{s^{2}}}\right)\left(\frac{1 \mathrm{~kJ}}{10^{3} N m}\right)$
$Q=-22.6 \mathrm{~kJ} / \mathrm{kg}$
$\left\{\right.$ Note: From Table A-4, @ $\mathrm{T}_{1}=400^{\circ} \mathrm{C}$ and $\mathrm{P}_{1}=30 \mathrm{bars}, \mathrm{h}_{1}=3230.9 \mathrm{~kJ} / \mathrm{kg}$ and $\mathrm{s}_{1}=6.9212 \mathrm{~kJ} / \mathrm{kg} \mathrm{K}$
From Table A-2, @ $\mathrm{T}_{2}=100^{\circ} \mathrm{C}$ and $\mathrm{x}_{2}=1, \mathrm{~h}_{2}=2676.1 \mathrm{~kJ} / \mathrm{kg}$ and $\left.\mathrm{s}_{2}=7.3549 \mathrm{~kJ} / \mathrm{kg} \mathrm{K}\right\}$

Entropy Balance (Second Law of Thermodynamics):

$$
\begin{align*}
& \frac{\dot{Q}}{T_{b}}+\dot{S}_{g e n}=\dot{m}\left(s_{2}-s_{1}\right)  \tag{2.5}\\
& \frac{\dot{S}_{g e n}}{\dot{m}}=\left(s_{2}-s_{1}\right)-\frac{\left(\frac{\dot{Q}}{\dot{m}}\right)}{T_{b}}  \tag{2.6}\\
& S_{\text {gen }}=(7.3549-6.9212)\left(\frac{\mathrm{kJ}}{\mathrm{~kg} \mathrm{~K}}\right)-\frac{(-22.6)\left(\frac{\mathrm{kJ}}{\mathrm{~kg}}\right)}{500 \mathrm{~K}}  \tag{2.7}\\
& S_{\text {gen }}=0.4789 \mathrm{~kJ} / \mathrm{kg} \mathrm{~K}
\end{align*}
$$

